

Refining Industry of Mexico

Comparative study of R&D activities and the catalysts market needs

José Manuel Domínguez, Jaime Aboites, Tomas A. Beltrán and Rodolfo Quintero

There are some factors that might disrupt the value chain for transferring new catalysts technology to the main processes of the refining industry. The main driving forces of the refining industry of today include the declining quality of crude and the more stringent environmental regulations. Both factors are thought to play a directing role for R&D activities in the field of catalysis, and have an impact on technological and economical issues. Also, within the R&D centers both organizational and economical aspects influence the relationship between the real catalysts market needs and the specific R&D projects.

The main driving forces of the catalysts industry for refining processes in the past decades were the continuous improvement of the production volume, costs/profit ratios and catalyst activity steadiness [1-3]. However, in recent years two additional forces playing a directing role are the declining quality of crude available and the strict environmental regulations [4, 5]. The former factor brings out important technical and economical challenges to refiners, such as the transformation of heavier oil fractions having a specific density lower than 22 °Api, a high sulfur content up to about 3 to 4 wt% and metals loading up to 100-250 ppm (Ni, V).

In addition, the asphaltenes concentration in this type of crude may rise up to 3 to 5 wt%, while the carbon weight percentage remains around 10%. The second factor motivated the development of technological issues in all the processes of the refinery to comply environmental regulations, by means of the removal of precursors of the most harmful fuel emission compounds such as sulfur, nitrogen, aromatics and olefins [5]. The goals set up by the US environmental regulations for the year 2006 establish a sulfur content in gasoline of less than 30 ppm, that is an order of magnitude less than the current figure, while the total aromatics content is targeted at 10 vol.% and the benzene limits set down to less than 1% vol. In addition, the trends in Reid vapor pressure of gasoline point out to less than 7 psi (1 psi = 6894.76 Pa) [5-8]. Then, to reach these goals a twofold strategy based upon serious improvements of the refining processes and the development of new catalysts must be considered.

In this context, the refining industry of Mexico faces important

challenges such as the upgrading of heavy Maya crude, the fulfillment of international standards in terms of fuels quality and post-combustion gas treatments, in order to reduce the levels of contaminants in the populated areas.

To this end, the options available include the upgrading of refinery process as well as the development of new catalysts. The latter issue is considered as a precious alternative instead of modifying the actual plants that should incur in further capital investments. For example, new hydrotreating catalysts supports having outstanding properties [9] should offer a significant performance with respect to traditional Al_2O_3 -supported NiMo or CoMo catalysts, which now operate under more severe temperature and pressure conditions, which in turn accelerates the catalysts deactivation rate. Also, innovative concepts such as the deposition of active microphases into the confined space of nanoporous materials is thought to give control in defining new reaction pathways for processing complex hydrocarbon molecules [10, 11].

In both cases, innovation through research must play a key role to keep abreast with the constant requirements of the refining industry. In summary, new catalysts are needed for dealing with the highly polluted crude fractions, while keeping the product quality within the stringent environmental regulations. In other industrial areas, such as the petrochemicals and chemical products industries, the monetary value of the catalysts market is even higher with respect to the oil refining industry, i.e., the market forecast for polymerization catalysts indicates a market growth rate of about 25% for the incoming years [12].

Thus, in this document we compare some of the actual needs of the refining industry of Mexico and how they compare with the recent research efforts made under both academy- and technology-driven research centers in the field of catalysis and how the researchers face the new challenges posed by the factors mentioned above.

J.M. Domínguez, T.A. Beltrán, R. Quintero, Instituto Mexicano del Petróleo (IMP) - Molecular Engineering Program/Competency of Catalysis - Eje Central L. Cárdenas 152 - 07730 México D.F.; J. Aboites, Metropolitan Autonomous University-Xochimilco - Calzada del Hueso 1100 - Col. Villa Quietud, Delegación Coyoacan, Mexico D.F. jmdoming@imp.mx

Types of crude oils and internal market demand

Most of Mexican crude oil originates from the coastal region off-shore around the Gulf of Mexico, where at least four types of crude prevail according to their composition and density (i.e., °Api). For example, Maya crude has a typical specific density of about 22 °Api, as illustrated in Table 1. In comparison, the typical density of crude processed in most of US refineries is close to 34 °Api [13]. Also, Table 2 indicates that Mexican Maya crude is rich in sulfur, asphaltenes, carbon and metals (Ni, V), which poses important technical challenges for their extraction, transportation and processing [14]. The latter point is particularly sensitive in terms of the yields of gasoline, intermediate distillates, gas oil feeds to FCC and residuals from Maya crude.

For example, these yields are about 15, 25.5, 22 and 37.5 vol.%, respectively, while lighter crude such as Itsmo oil yields about 23.8, 33.6, 25.3 and 17.3 vol.%, respectively. On the other hand, PEP total production is shared between internal market and exports as indicated in Table 3 and Table 4. The main trends observed here are the gradual increase of heavy oil destined to internal market (i.e., 11.3 and 24.5% in 1998 and 1999, respectively) and the step diminution of light oil (Itsmo + Olmeca) for exports (i.e., -3.3 and -10.8% for 1998 and 1999, respectively). Without a previous treatment 100% Maya feeds are not practical for processing by the actual refining plants, that is why blends containing about 70% Itsmo and 30% Maya are being more common in most of the refining system, as indicated in Table 5, where one observes a dramatic effect on the vacuum residuals derived from those feeds, which poses serious technical limits for further processing.

On the other hand, several factors influence the process configuration of most of the refineries, the main global factors being the crude quality and its composition, the market needs, the technology available and the capability for financial investment. In Latin American countries the refining scheme is variable as indicated in Figure 1, as their catalysts market structure is in consequence. Here one observes that the annual catalysts market value for the region amounts about 210 million US\$, according to data corresponding to year 2000 [12], which represents about 7.6% of the total refining catalysts market on a worldwide basis. In particular, Mexico represents about 31% of the Latin American market (Table 6) or about 2% of the worldwide market (Table 7). As observed in these data, the main processes involved are hydrocracking, FCC and hydrotreating, but substantial differences occur in the market structure of each country with respect to the other. For example, in Mexico the hydrocracking process catalysts market represents about 50% on a monetary basis, while Venezuela and Brazil do not include that processes in their refining scheme. It is worthwhile mentioning the marginal importance of the reforming process in countries like Brazil and Colombia. In comparison, the specific weight of the catalyst market in the Usa, Europe, Japan, anterior Urss and Canada represents each about 42, 22, 7.2, 5.25 and 3.5% of the worldwide catalyst market for refining, respectively.

The refining capacity worldwide is indicated on Table 7. It is interesting noticing how the capacity of the refining system in Mexico compares with other countries, for example the 6 refineries of Mexico produce about 80% of the total refining capacity of Canada or Australasia, who count on 21 and 19 re-

Table 1 - Density of Mexican crude oils

| Type of crude* | Specific density (°Api) | Density (gr/cm ³) | National Market | International Market (Types) |
|----------------|-------------------------|-------------------------------|-----------------|------------------------------|
| 10.0 | > 1.0 | | Extra heavy | Shale oil, bitumen etc. |
| D≤22.3 | 1.0-0.92 | | Heavy | Maya, Altamira |
| 22.3<D<31.1 | 0.92-0.87 | | Mean | Blends |
| 31.1< D<39 | 0.87-0.83 | | Light | Itsmo |
| >39 | <0.83 | | Super light | Olmeca |

* PEP (Pemex-Exploration & Production) Annual report (2001), Vol. 3, 18.

Table 2 - Comparison of the properties of some heavy crude oils

| | Arabian Light | Heavy | Maya Mexican | Derived oil Coal | Bitumen |
|-------------------------|---------------|-------|--------------|------------------|---------|
| Specific Density (°Api) | 34.4 | 28.2 | 22 | 27.4 | 22.9 |
| Sulfur (wt%) | 1.7 | 2.8 | 3.3 | 0.1 | 0.6 |
| Nitrogen (wt%) | 0.04 | 0.09 | 0.1 | 0.19 | 1.51 |
| Asphaltene (wt%) | 1.7 | 4.6 | 5.2 | 0.1 | 0.3 |
| Carbon (wt%) | 3.6 | 7.9 | 10.3 | 0.1 | 1.4 |
| Ni/V (ppm) | 4/13 | 18/56 | 35/174 | 1/1 | 6/1 |

Table 3 - Internal market distribution of oil produced by PEP in the period 1997-99*

| Crude type | 1997 (10 ³ B/D)** | 1998 (10 ³ B/D) | 1999 (10 ³ B/D) |
|--------------|---------------------------------|-------------------------------|-------------------------------|
| Heavy | 449 | 500 | 559 |
| Light | 796 | 798 | 760 |
| Super light | 22 | 19 | 20 |
| Total | 1,267 | 1,318 | 1,339 |

* PEP (Pemex-Exploration & Production) Annual report (2001), Vol. 3, 22.

** B/D = Barrels per day

Table 4 - Total annual exports of the oil produced by PEP in 1997-99* (m 10³ B/D)**

| Crude Type | 1997 | 1998 | 1999 |
|--------------|--------------|--------------|--------------|
| Altamira | - | 6 | 9 |
| Maya | 1,020 | 1,057 | 919 |
| Itsmo | 216 | 208 | 190 |
| Olmeca | 485 | 470 | 435 |
| Total | 1,721 | 1,741 | 1,554 |

* PEP (Pemex-Exploration & Production) Annual report (2001), Vol. 3.

** B/D = Barrels per day

Table 5 - Properties of a typical feed blend (Maya/70/30) and vacuum residuals*

| Properties | Crude blend (70% Itsmo, 30% Maya) | Vacuum residuals |
|--------------------------|--------------------------------------|------------------|
| Specific Density (°Api) | 30.4 | 6.6 |
| Sulfur (wt%) | 2.07 | 4.6 |
| Asphaltene (wt% in n-C5) | 6.35 | 22.1 |
| Ni (ppm) | 21.3 | 73.4 |
| V (ppm) | 127.4 | 439.1 |

* PEP (Pemex-Exploration & Production) Annual report (2001), Vol. 3.

Table 6 - Catalysts market size in Latin America (monetary basis)

| Catalysts market | Mexico | Venezuela | Brazil | Argentina | Colombia | Other |
|------------------|--------|-----------|--------|-----------|----------|-------|
| million US\$ | 65 | 43.1 | 41.7 | 21.7 | 8.4 | 29.6 |
| % | 31 | 20.6 | 19.85 | 10.35 | 4.0 | 14.2 |

fineries, respectively. Also, the treatment of residuals by thermal coking is 41 MB/D for Mexico and 40 MB/D in Canada, while two of the major processes for obtaining automotive fuels, i.e., FCC and alkylation, are about 368 vs 417 and 62 vs 121 MB/D, for Mexico and Canada, respectively.

Research and development of catalysts

The petroleum industry of Mexico has a significant technological support in the Instituto Mexicano del Petroleo (IMP), i.e., the Mexican Petroleum Institute, which concentrates about five thousand people working on different areas of engineering, oil extraction, technical services related to production maintenance etc., and some areas of research and development. The latter are distributed in eight programs comprising about 450 people with more than a half of them holding a PhD degree. About 15% of these people work on eight catalysis research projects, which are carried out within the framework of two research programs, the "Molecular Engineering" and "Maya Crude Treatment" programs. These activities absorb about 20% of the total investment on R&D activities at IMP, that is about 4.5 million US\$ (i.e., comprising manpower, utility services, equipment cost depreciation, materials, displacements etc). In addition, there is a task force of about one hundred people who are devoted to pilot plants operation and technical services required by the oil refining industry in all matters related to catalysts operation. The latter group works on a cost/benefits scheme through specific contracts with Pemex-Refinación, i.e., the national refining industry. The main topics of research are listed on Table 8.

In addition, since 1997 a special program, called FIES, is be-

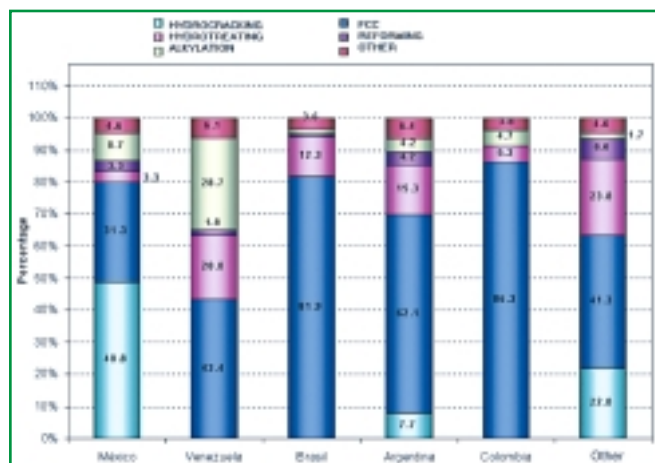


Figure 1 - Catalysts market structure of Latin America for oil refining

ing carried out in close collaboration with academic groups from some universities and other research centers. The evaluation of the proposals is carried out by specific committees comprising academic and petroleum industry people, then a proper financing of the projects is established and taken in charge by IMP. The main partners representing the strongest groups working on catalysis research are the Metropolitan University (UAM-Iztapalapa), the National University (UNAM), the National Polytechnic Institute (IPN), the Center for Advanced Materials Research (CIMAV) and the Technological Institute of Madero City (ITCM). In terms of scientific production the catalysis community in Mexico participates in several forums where two are considered the most significant from the regional viewpoint, those are the North American Catalysis Society Meeting and the Ibero-American Catalysis Symposium. Both of these events are carried out every two years and the last ones were at Toronto (Canada) in June 2001 (NACS 2001) and Porto (Portugal) in 2000 (Simposio Iberoamericano de Catálisis 2000). If one takes these events as the most representative of the main stream of catalysis research work going on in Mexico, then a statistics emerges for

Table 7 - Refining capacity worldwide (MB/D)*

| Country | No. Refineries | Total refining | Vacuum distillation | Coker | TCC | FCC | Reforming | HDT | HDC | Alkylation | Other |
|----------------|----------------|----------------|---------------------|-------|-------|-------|-----------|--------|-------|------------|-------|
| Usa | 152 | 16,538 | 7,468 | 2,100 | 64 | 5,588 | 3,559 | 10,856 | 1,441 | 1,170 | 1,403 |
| Canada | 21 | 1,906 | 629 | 40 | 136.5 | 415 | 350 | 814 | 258 | 62 | 164 |
| Mexico | 6 | 1,525 | 757 | 41 | - | 368 | 226 | 748 | 68.5 | 121 | 41.3 |
| (Rest) | | | | | | | | | | | |
| Latin American | 70 | 6,676 | 2,816 | 397 | 435 | 1,115 | 403 | 1,832 | 162 | 99 | 175 |
| Europe | 132 | 16,088 | 5,762 | 413 | 1,662 | 2,424 | 2,385 | 8,629 | 912 | 241 | 1,010 |
| Anterior URSS | 59 | 8,399 | 2,780 | 217 | 413.5 | 511 | 1,137 | 3,127 | 68 | 12 | 205 |
| Middle East | 51 | 6,686 | 2,164 | 87 | 430 | 334 | 623 | 1,965 | 634 | 29 | 151 |
| Asia | 24 | 2,467 | 517 | 50 | 116.5 | 167 | 62 | 212 | 55.8 | - | 27 |
| China | 97 | 4,346 | 40 | 290 | - | 892 | 157 | 283 | 122 | 26.5 | 50 |
| Japan | 35 | 4,962 | 1,651 | 88.5 | - | 799 | 720 | 4,261 | 162 | 43 | 211 |
| Australasia | 19 | 1,945 | 470 | 32.6 | 59 | 331 | 318 | 461 | 129 | 35.6 | 72 |
| Other | | | | | | | | | | | |
| Asia-Pacific | 30 | 6,444 | 1,040 | 53 | 248 | 436 | 718 | 2,605 | 263 | 12.6 | 268 |

* MB/D = thousands of barrels per day

Table 8 - Main catalysis R&D projects at IMP*

| R&D project | Program |
|--|-----------------------|
| Synthesis and properties of micro- and mesoporous materials for oil refining | Molecular engineering |
| Development of catalysts for sulfur reduction in gasoline | Maya crude treatment |
| Development of catalysts for sulfur reduction in diesel | Maya crude treatment |
| New catalytic systems for FCC reactions | Maya crude treatment |
| New catalytic systems for CCR naphtha reforming | Maya crude treatment |
| Synthetic crude production by HDT and hydrocracking | Maya crude treatment |
| High octane gasoline by light olefin dimerization and I-C4 alkylation | Maya crude treatment |
| Catalytic monoliths for stationary emission of pollutants | Molecular engineering |

with respect to the total production) were made in cross collaboration among all the partners.

When considering the refining market needs, it arises another interesting question, that is about the main topics of research presented in the forums mentioned above. These should reflect the main focus of catalysis research, but this information could be

biased by several factors such as the novelty of the topic in the international scientific journals, the main financing currently established by the FIES program itself, the particular interests of researchers on a specific topic issued from their previous PhD work and last, but not least, from the market needs. Then, Figure 3 is a summary of the main topics found in the analysis of 158 papers presented during the period 1998-2001 in the four events mentioned above [12].

Main resources and perspective of catalysts development

In 1985 the Pimentel Report presented before the US Research Council [19] a survey of the most important technologies, where catalysis was defined as "one of the five priority areas needed to keep industrial and economical leadership of the US". Then, a sustained endeavor was recommended to further develop the interaction between the basic research areas and their technological counterparts.

Nowadays, the infrastructure needed for performing world class catalysis research and development includes three main factors: the artwork needed for catalysts synthesis, the highly sophisticated machines and methods for the characterization of catalysts properties and the micro and pilot plant facilities for testing and scaling up the laboratory leads. All of this requires important economical resources for keeping up the facilities updated, as well as a sustained endeavor from qualified human resources. In this respect, the national catalysis R&D resources in Mexico comprise a variety of modern techniques located either in academic laboratories or at IMP, where most of the newer developments for industrial applications in this field come from. The main infrastructure needed for keeping up a competitive endeavor in innovative R&D projects exist at IMP and in other Mexican academic centers. Most of the modern techniques like NMR-MAS (Solid State), High Resolution Electron Microscopy and a Combinatorial Catalysis Robot (i.e. from Symyx Inc.) are available at IMP, together with sophisticated Pilot Plants for FCC, hydrocracking and HDT studies, but other techniques like XPS (X-Ray Photoelectron Spectroscopy) or Synchrotron related facilities are not available by now.

With respect to human resources (Figure 3), a significant part of the senior researchers working in the catalysis field obtained their PhD in Europe and Usa. At IMP, about one tenth of the total PhD's work on catalysis R&D programs. About 26 PhD's, 21 M.Sc.'s and 61 B.Sc.'s participate in the R&D projects and technical services, respectively, while about 49 people at IMP participate in the operation of microplants and pilot plants facilities, as well as other administrative endeavors.

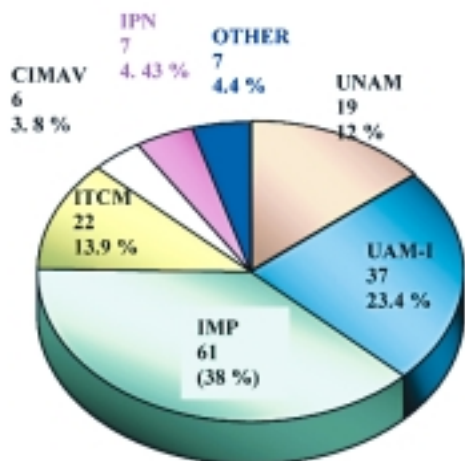


Figure 2a - Catalysis research production in Mexico (1998-2001)

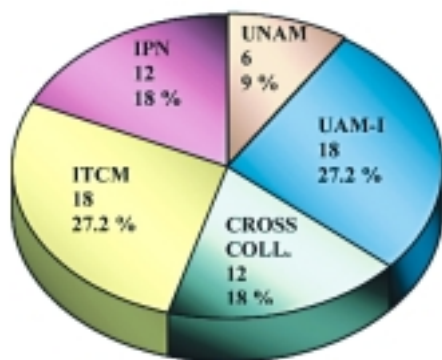


Figure 2b - Catalysis research collaboration between academic institutions with IMP [15-17]

the period 1998-2001 as shown in Figure 2a, which is the contribution of each institution to the forums mentioned above [15-18], from a total of 158 articles, where 47 belong to the Ibero-American Symposium of Porto in 2000, 40 articles were presented in the NACS Meeting in Toronto in 2001, 50 belong to the Ibero-American Symposium of Colombia in 1998 and 21 more were presented in the NACS Meeting held at Boston, Usa in 1999.

A total of 54 articles were found to include a collaboration of academic researchers with the scientific staff at IMP, that is about 34.1% with respect to the total production of the period 1998-2001 and a significant part of the 66 papers (i.e., 41%

Table 9 - Potential areas of opportunity in the refining industry in Mexico (period 2000-2006) [5]

| Opportunity areas | Process |
|--|--|
| Reduction of sulfur in gasoline (i.e., 30 ppm) | Hydrotreating of FCC feeds Gas oil HDS Hydrocracking |
| Reduction of sulfur in diesel (i.e., 30ppm) | Hydrotreating of FCC feeds Gas oil HDS Hydrocracking |
| MTBE phase out | Isoparaffins alkylation with olefines C ₄ -dimerization |
| Hydrogen production | Synthesis gas reforming |
| Improvement of catalysts performance | Minor deactivation Higher activity and selectivity Possible regeneration Minor costs |
| Catalytic processing of complex feeds (3.3% S, 0.1% N, 10.3% C, Ni/V=35/174 ppm, asphaltenes: 5.2 wt%) | HDS of naphtha, gas oil and residuals FCC Hydrocracking (H-OIL) |
| Improved gasoline: high octane number low vapor Reid pressure low aromatics | Isoparaffins alkylation with olefins Dimerization of light olefines Hydrocarbons isomerization Selective reforming Fischer-Tropsch Process |
| Synthetic crude | HDT Visbreaking Alternate processes (ultrasound, microwave etc.) |

Personnel Distribution

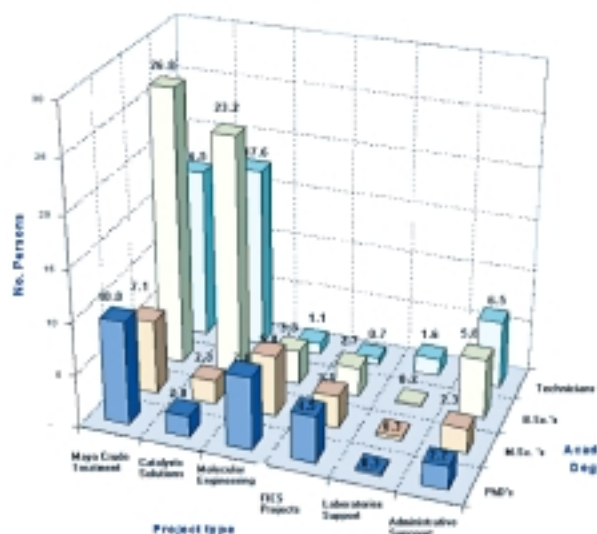


Figure 4 - Distribution of personnel working on catalysis at IMP

Conclusions

In this report a comparative study was presented between the needs existing in the refining industry of Mexico and the current R&D activities in both academic and technological centers in Mexico. The actual production of crude in Mexico comprises about 2,893 MB/D, which ranks in about 4th production place on a worldwide basis, where 1,339 MB/D are processed by the 6-Refinery Complex System of Mexico and about 1,554 MB/D are exported, mainly to the Usa. On the other hand, the annual growth in the international refining catalysts market is about 6.5%, to reach about 3,200 million US\$ in 2003 [12], which is equivalent to 7,600 million pounds on a weight basis, that is about 90% of the catalysts volume in a global scale, but it only represents about 45% of the catalysts total market in a monetary basis [3, 12]. The difference of 55% comes from petrochemicals and chemicals production market, which means less volume but more value in a monetary basis. Among the main opportunities existing nowadays in the refining industry are: 1) the production of low sulfur gasoline and diesel, targeted at about 30 ppm for 2006; 2) the integral processing of heavy crude and 3) the introduction of new gasoline additives due to the probable phase out of MTBE. These trends are the basis of a forecast on major opportunities in catalytic processes and they are summarized in Table 9.

The competition factors in the refining catalysts market are based upon a clear product differentiation with a market focus in mind, the low costs leadership, a proper market positioning, the joint ventures and a combination of manufacture-distribution and technical assistance.

It is worth noticing in Figures 2a and 2b that the main catalysis R&D endeavors in Mexico are focused on three main areas, i.e. hydrotreating catalysts (HDT), new catalytic materials (NCM) and solid acid catalysts (SAC). However, according to the catalysts consumption market the main emphasis is focused on the conversion of heavy residuals by hydrocracking and FCC catalytic processes, with smaller emphasis in hydrotreating and reforming processes. The latter represent on-

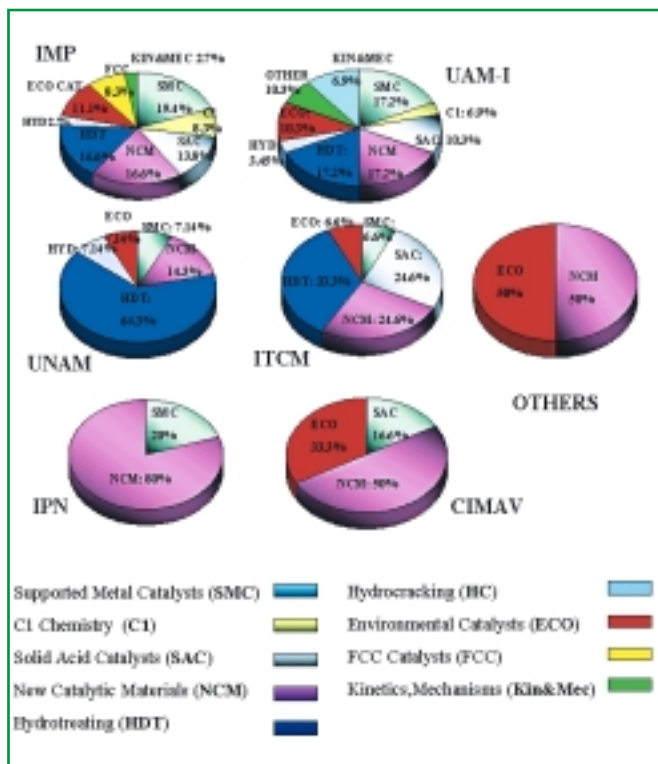


Figure 3 - Main topics of catalysis research in Mexican institutions (%) [15-17]

ly 3% each with respect to the actual market structure (Figure 1). Then, there is an asymmetric relationship between the actual catalysts market needs and R&D efforts that must be analyzed further in the light of future R&D projects. In addition, as indicated in Figure 3, the personnel working in catalysis show a significant dispersion over three distinct platforms, which might pose organizational barriers for these groups to achieve common goals along the value chain comprising the areas from basic research to industrial applications.

References

- [1] J.H. Gary, G.E. Handwerk, *Petroleum Refining: Technology and Economics*, 3rd Ed., Marcel Dekker, New York, 1994.
- [2] F. Bel, B. Bourgeois, *Innovation Direction and Persistence within an Industry: the Refining Processes*, Eur. Meet. Appl. Evolutionary Economics, Grenoble (France), June 1999, 1.
- [3] G. Martino, "Catalysts for Oil Refining and Petrochemistry, Recent Developments and Future Trends, Proc. 12th International Congress on Catalysis, Granada (Spain), July 2000, *Studies in Surface Science and Catalysis*, 2000, **130**, 83.
- [4] a) M. Kulakowsky, *Reformulated Gasoline: Defining the Challenge*, ACS Symposium on the Impact of Reformulated Fuels, ACS Division Petr. Chem. Prepr., 1994, **39**, 494; b) J.W.N. Sonnemans, *Catalysis in Petroleum Refining and Petrochemicals Industry 1995*, M. Absi-Halabi *et al.* (Eds.), *Studies in Surface Science and Catalysis*, Elsevier Science, The Netherlands, 1996, **100**, 99.
- [5] M. Absi-Halabi *et al.*, *Hydr. Proc.*, 1997, February, 45.
- [6] H.J. Lovink, *Symposium on the Impact of Reformulated Fuels*, 208th ACS Meeting, Div. Petr. Chem., 1994, August, 513.
- [7] a) A.P. Lamourelle *et al.*, *Clean Fuels: Route to Low Sulfur Low Aromatic Diesel*, NPRA 2001 Annual Meeting, March 18-20, 2001, New Orleans (LA, Usa), 2001, AM-01-28; b) T.R. Eizember, *Diesel Sulfur Regulation Potential for Disruptions in the Marketplace*, NPRA 2001 Annual Meeting, March 18-20, 2001, New Orleans (LA, Usa), 2001, AM-01-62.
- [8] a) W. K. Shiflett, *Producing the Environmental Fuels of the Future*, NPRA 2000 Annual Meeting March 26-28, 2000, San Antonio (TX, Usa), 2000, AM-00-15; b) J.L. Nocca, *The Domino Interaction of Refinery Processes for Gasoline Quality Attainment*, NPRA 2000 Annual Meeting March 26-28, 2000, San Antonio (TX, Usa), 2000, AM-00-61.
- [9] F. Luck, *Bull. Soc. Chim. Belg.*, 1991, **100**(11-12), 781.
- [10] S. Seelan *et al.*, *Effects of Molecular Confinement on Structure and Catalytic Behaviour of Metal Phthalocyanine Complexes Encapsulated in Zeolite-Y, Zeolites and Mesomorphous Materials 14-P-12* (2001), *Studies in Surface Science and Catalysis*, A. Galarneau *et al.* (Eds.) Montpellier, April 12, 2001.
- [11] H. Yoshitake *et al.*, *Structure of Mo Species Incorporated into SBA-1 and SBA-3 Studied by XAFS and UV-VIS Spectroscopies*, *Zeolites and Mesomorphous Materials*, 14-P-26, 2001, *Studies in Surface Science and Catalysis*, A. Galarneau *et al.* (Eds.), Montpellier, April 12, 2001.
- [12] The Freedonia Group Inc., *Chem. & Petr. Catalysts, Industry Study*, 1178, 1999.
- [13] J.R. Doshier, J.T. Carney, *Oil & Gas Journal*, 1994, May 23, 43.
- [14] E.J. Swain, *Oil & Gas Journal*, 1995, Jan. 9, 7.
- [15] North American Catalysis Society Meeting, NACS, Boston, Ma, 1999.
- [16] Iberoamerican Catalysis Symposium, Cartagena de Indias, Colombia, 1998
- [17] North American Catalysis Society Meeting, NACS, Toronto, Canada, 2001.
- [18] Iberoamerican Catalysis Symposium, Porto, Portugal, 2000.
- [19] Pimentel *et al.*, *Opportunities in Chemistry*, National Academy Press, 1985

Acknowledgments. We appreciate the financial support of IMP through the FIES-98-66-V project and to Dr. G. Chapela, IMP General Director, for the facilities given during the sabbatical stage of one of the authors (JA).